ERRATA BSL-II 8 ptg **Dated 6 Jun 06**

Line 5a = line 5 from above; Line 7b = line 7 from below

Page	Location	Reads	Should Read
iv	Addendum	University of Puerto	University of Puerto Rico
iv	Addendum	Carlos Ramirez (no accent on "i")	Carlos A. Ramírez (accent on "í", and add middle initial)
12	fn 2, line 3	*Mathematica* (1687)	*Mathematica*, London (1687)
14	Table 1.1-1, col 3	gm	g
19	line 6b	of the lesser *y*	of lesser *y*
20	Fig 1.2-2(a), 2nd figure	Delete the spurious arrowhead above the cylinder next to the *y* coordinate	
20	Fig 1.2-2(a), 3rd figure	*z*-direction $(\pi/z)-\alpha$	+*z*-direction $(\pi/2)-\alpha$
20	Fig 1.2-2(b) top figure	Add an arrow to indicate the theta-direction	
20	Fig.1.2-2(b)	Top dwg: θ-direction Middle dwg: ϕ-direction Bottom dwg: *r*-direction	$+\theta$-direction $+\phi$-direction + *r*-direction
37	Qu. 12, line 1	about kinetic	about the kinetic
38	1B.1, line 4	for the Newtonian	for a Newtonian
39	1C.1(c), line 1	by	from
39	Prob 1C.3, line 4	…wall.	…wall, assuming specular reflections.
39	Fig 1D.2	**f** (in drawing)	π_n
40	3b	*steady flow*	*steady, rectilinear*

[Thanks to Professor Chih-Hsin James Shih, Feng Chia University, Taichung, Taiwan]

42	Item "a"	…condition."	…condition." See Problem 2D.3 for further ideas.
46	6 lines after Eq 2.2-23	regime	regimes
50	2 lines above Eq 2.3-14 [from Meshach Prasanna Heenatigala]	Appendix B.2	Appendix B.1
62	2A.3, line 4	lb/ft^3	lb_m/ft^3
62	2A.4, line 5	$0.045\ \text{lb}/\text{ft}^3$	$0.045\ \text{lb}_m/\text{ft}^3$
65	2B.8, line 1	lb/hr	lb_m/hr
66	1 line after 2B.9-2	$p_{\text{avg}} = \frac{1}{2}(p_0 - p_L)$.	$p_{\text{avg}} = \frac{1}{2}(p_0 - p_L)$, and ρ_{avg} is the average density calculated at p_{avg}.
67	line 2a	in the above equation	in Eq. 2B.10-1
67	line 2a	the equation becomes	it becomes
69	Figure caption	The figure caption should read: "A possible particle trajectory. The particle that begins at $z=0$, $x=B$ and ends at $x=-B$ may not necessarily travel the longest distance in the z-direction." [from Bahman Homayun]	
73	2C.7, ans. (c)	t_0	t_{rel}
74	Add Prob 2D.3	**2D.3 The no-slip condition at solid walls** Read S. Richardson, *J. Fluid Mech.*, **59**, 707-719 (1973), and discuss the physical meaning of the no-slip condition.	
81	1line above 3.3-1	…*energy*:	…*energy* for symmetrical τ (see Eq. 1.2-4):
92	Fig 3.6-3, caption	Fig. 3.5-4(*b*)	Fig. 3.6-4(*b*)
93	fn 5, line 4	…edition (2000).	…edition, Springer-Verlag,

			Berlin (2000).
104	3A.3, answer	… $\mathrm{N/m^2}$	,,, $\mathrm{N/m^2}$ (if $\rho = \rho(p)$)
105	3A.5, line 4	hardens.	hardens (see Fig. 3.6-6).
105	Fig 3A.7	$T = 60'$	$D = 60'$
105	3B.1(a), line 6	exerted by the two	exerted on the fluid by the two
106	Eqs 3B.4-4, 5, 6	ln cot	ln cot
111	Prob 3C.2	example	Example
124	lines after 4.2-6	recognizing [to avoid splitting up $\cos\theta$]	noting
125	addn to fn 4	…760 (1969). A solution to the unsteady-state analog of Eq. 4.2-2 was obtained by F. Sy, J. W. Taunton, and E. N. Lightfoot, *AIChE Journal*, **16**, 386-391 (1970).	
132	Fig caption	$c[(2/(2-\beta)]$	$c[2/(2-\beta)]$
133	Fig caption	…empty region.	…empty region, shaded gray.
140	Eq 4.4-35	$(1 + f'^2)$	$(1 - f'^2)$
142	Prob 4A.6(c)	of the plate	on the plate
142	4B.2, line 2	Example 4.1.1	Examples 4.1-1
144	line 4a	unit normal on	unit vector normal to
145	4C.1, line 4	$0 < x < L_e$	$0 \le x \le L_e$
145	Eq 4C.1-1	$0 < y < \delta$	$0 \le y \le \delta$
145	Eq 4C.1-2	$\delta < y < \mathrm{B}$ (with roman B)	$\delta \le y \le B$ (with italic B)
146	1 line above 4C.1-3	$0 < x < L_e$	$0 \le x \le L_e$
148	Prob 4C.2(f)	ϕ°	$\phi^{\circ}(x)$

148	Prob 4C.2(j)	2500 gmcm^2	2500 g cm^2
148	Prob 4C.2(j)	4×10^6 dyn cm$\rho =$ 1gm/cm^3, $(a-1)R = 10^{-2}$ cm.	4×10^6 dyn cm, $\rho =$ 1g/cm^3, and $(a-1)R = 10^{-2}$ cm.
168	Eq 5.5-10	485	477
168	3 lines above ex.	Fig. 5.4-3	Eq. 5.4-3
169	Eq 5.6-8	at $z = \infty$, $\bar{v}_z = 0$	as $z \to \infty$, $\bar{v}_z \to 0$
173	last line of 5C.1	…for the fluid.	…for the fluid, and J is the total momentum flow defined analogously to Eq. 5.6-2.
174	line 1a	Eq. 5.4-2	Eq. 5.4-3
174	Prob 5C.1(j)	line z = constant	plane z = constant
175	line 4a	$r < br$ $r > br$	$r \le br$ $r \ge br$
180	fn 1, line 1	$(\partial^2/\partial \breve{z}^2)\mathbf{v}$	$(\partial^2/\partial \breve{z}^2)\breve{\mathbf{v}}$
180	fn 1, line 3	$\mathbf{v}$	$\breve{\mathbf{v}}$
182	Eq. 6.2-13	$\log_{10}\mathrm{Re}\sqrt{f}$	$\log_{10}(\mathrm{Re}\sqrt{f})$
183	Ex 6.2-2, line 1	in pounds per hour	in $\mathrm{lb}_m/\mathrm{hr}$
185	line before 6.3-5	definition in Eq. 6.1-5,	definitions in Eq. 6.1-5 and Eq. 3.7-4,
185	Eq 6.3-5	$\left(-\left(\breve{\mathscr{P}} - \breve{\mathscr{P}}_0\right)\Big\vert_{\breve{r}=1} \cos\theta\right)$	$\left(-\breve{\mathscr{P}}\Big\vert_{\breve{r}=1} \cos\theta\right)$
185	Eq 6.3-7	$\breve{\mathscr{P}} - \breve{\mathscr{P}}_0$	$\mathscr{P} - \mathscr{P}_0$
185	Eq 6.3-10	at $\breve{r} = \infty$, $\breve{v}_z = 1$	as $\breve{r} \to \infty$, $\breve{v}_z \to 1$

185	Eq 6.3-11	at $\breve{r} = \infty$, $\mathscr{P} = 0$	as $\breve{r} \to \infty$, $\mathscr{P} \to 0$
193	6A.2(b)	drop is	drop (pump outlet to reservoir) is
193	6A.6, line 6	lb/min	lb_m/min
194	6A.8, line 4	lb/ft^3	lb_m/ft^3
196	6C.3-2	$-\mu$	$+\mu$
203	Fig 7.3-1, side view	Delete: r_2	Add: $\mathbf{r}_2$ as label to the vertical arrow just above the vertical arrow for $\mathbf{u}_2$
203	Fig 7.3-1, top view	r_1	$\mathbf{r}_1$
205	last line of §7.4	Eq. 7.4-10	Eq. 7.4-11
207	Eq 7.5-10	$g(z_2 - z_1)$	$g(h_2 - h_1)$
212	line 1 of solution	3-in. pipe	4-in. pipe
212	Eq 7.6-18	(3 × 2.54)	(4 × 2.54)
212	Eq 7.6-18	3×10^6	2.3×10^6
213	Eqs 7.6-27 & 28	$\dfrac{(120)^2}{2(0.049)(32.2)}$	$\dfrac{(120)^2}{60(0.049)(32.2)}$
213	Eq 7.6-27 line 3	(144)	(114)
217	Lines 1a and 2a	At time $t = 0$	For all times $t > 0$
218	Eq 7.7-7	$\sqrt{2gH}$	$-\sqrt{2gH}$
224	7A.1, line 2	0.0384 [Thanks to Jack Guidarelli at Iowa State University]	0.0284
225	Fig 7A.6	Internal diameter of all pipe is 5”	Internal diameter of all pipe segments is 5”

226	line 4a	7.5-6	7.5-7
226	Prob 7B.2, add to end of problem:	See pp. 14 and 15 of reference to R. B. Bird on p. 70.	
236	line 3a	…direction).	…directions).
257	1 line after 8.6-15	…quadratic in $\dot{\varepsilon}$ from	…quadratic in $\dot{\varepsilon}$, from
258	8A.2 line 6	the mass flow rate	the total mass flow rate
267	3 lines after 9.1-2a	T [=] C	T [=] ^{o}C
269	Table 9.1-1, rows 2, 4, and 5	C F	^{o}C ^{o}F
271	Table 9.1-4, 5^{th} col	Prandtl number[c]	Prandtl number
288	9A.10, line 2	predict thermal	predict the thermal
292	Eq 10.2-2 [from Eric A. Pohl, Columbia University]	$(2\pi rL)q_r\|_r)$	$(2\pi rL)(q_r\|_r)$
298	below 10.3-21	"To find the maximum, etc." needs to be moved down, by applying a "return" command.	
307	Figure	Change the directions of the *y* and *x* arrows	
308	fn 2,line 1	the *Biot*	a *Biot*
309	Ex 10.7-1, lines 5,6	F	^{o}F
310	after Eq 10.7-19	10 F^{o}	10 ^{o}F
313	Line 1a	The $\mu(\partial v_z/\partial_r)^2$	The term $\mu(\partial v_z/\partial r)^2$
323	10B.7 line 4	$z > 0$	$z \geq 0$
324	10B.8(iii) line 1	Heat loss	The heat flux
326	after Eq 10B.13-1	$k_{z,\text{eff}}$	$\kappa_{zz,\text{eff}}$
326	Figure	The symbol "*r*" with no subscript should be removed	

329	10C.1(a), line 3	position dependent	position-dependent	
331	fn 5, line 3	223-227	223-227).	
347	Fig. caption	…body of fluid.	…body of fluid at temperature T_1.	
348	Eq 11.4-48	$\eta \to \infty$	$\eta \to \pm\infty$	
352	Fig 11.4-5	λ_1	λ	
352	Figure	530 R	530 $^{\circ}$R	
356	5 lines above 11.5-10	at $x =$	as $x \to$	
356	11.5-12	at	as	
357	Figure, part (a)	System II	System I	
360	Example, line 3	tank surface temperature	bulk liquid temperature	
362	11A.4 answer	sec	s	
362	11A.5(a)	initial	upstream	
362	11A.5, ans (b)	888 R	888 $^{\circ}$R	
363	1 line after 11B.2-2	for all z	for all $z > 0$	
365	11B.7, tabulation	lb	lb_m	(twice)
365	11B.7, tabulation	F	$^{\circ}$F	(twice)
366	11B.9(e)	sec	s	
367	Eq 11B.12-1	$(\exp\theta_0 - \exp\theta)$	$(\exp\Theta_0 - \exp\Theta)$	
371	Eq. 11C.6-5	The 2 lower-case pi's here should be boldface and should look exactly like the pi to the right side of the equals sign in Eq 1.7-2		
372	11C.7(a), line 4	on system	on the	
389	Eq 12.4-15	$\Delta < 1$	$\Delta \le 1$	

395	12A.1, ans (b)	sec	s
396	12A.6(b), line 2	sec	s
396	12.B-1, table	$T(\mathrm{C})$	$T(^{\circ}\mathrm{C})$
397	fig caption	a film falling down	a liquid film flowing down
398	12B.4-5	$T = T_0$ $y = \infty$	$T \to T_0$ $y \to \infty$
398	2lines after 12B.4-6	at $y = \infty$	as $y \to \infty$
398	12B.4(f)	flux to	flux from the wall to
398	12B.5, line 2	For time $t > 0$	For all times $t > 0$
401	12C.3, line 2	For time $\underline{t} \geq 0$	For all times $t > 0$
401	Fig 12C.3 (left)	$t < 0$	$t \leq 0$
402	after Eq 12C.4-5	$\overline{T} - \overline{T}_0$	$\overline{T} - T_0$
406	Line after 12D.7-3	$\Gamma(a,x) = \int_0^\infty t^{a-1} e^{-t} dt$	$\Gamma(a,x) = \int_x^\infty t^{a-1} e^{-t} dt$
406	after Eq 12D.7-3	gamma functions.	gamma functions.[13]
406	above Eq 12D.8-1	for $\Delta > 1$ is[13]	for $\Delta \geq 1$ is[14]
406	footnotes	[13] H. Schlichting… [14] M. Abramowitz… [[Then put the footnotes in the proper order]]	[14] H. Schlichting… [13] M. Abramowitz…
415	Eq 13.5-7	at $r = \infty$, $\Theta = 0$	as $r \to \infty$, $\Theta \to 0$
417	fn 3	*AIChE Journal* (to be submitted).	(unpublished).
421	13D.1(b)	in laminar developed flow	in fully developed laminar flow
434	Eq 14.3-7	$0 \leq \breve{r} \leq \frac{1}{2}$	$0 \leq \breve{r} < \frac{1}{2}$

437	Eq 14.3-18	]	)
446	Figure 14.7-1	Remove the horizontal line to the right of the origin of coordinates. Remove the horizontal line just above the T_d	
450	14A.1 line 2	pounds per	pounds mass per
450	14A.2 line 2	pounds per	pounds mass per
451	14B.5, line 2	15.4-2	15.4-1
451	line 3a, left col	$T(\mathrm{C})$	$T(^\circ\mathrm{C})$
452	below 14D.1-5	A.7-13 and 14	A.7-14 and 15
457	Fig caption, line 3	ruled	lightly shaded
459	Fig 15.3-1	sec^{-1}	s^{-1}
459	line 2a, Ex 15.3-1	sec	s
459	1 line below 15.3-1	R	$^\circ\mathrm{R}$
464	line 5b	100 psi	100 psia
470	lines 1a & 2a	$<$	$\leq$
470	1 line above 15.5-18	$<$	$\leq$
476	15A.7(b)(iv)	inner pipe surface area	inner surface area of the inner pipe
477	above 15B.2-2	Eq. 6.2-13	Eq. 6.2-12
478	15B.3(c), line 3	"mass velocity"	mass flux
480	15B.6(d), line 1	fluid velocity	the fluid velocity
480	15B.6 answer	$\mathrm{ft\,sec}^{-1}$	$\mathrm{ft\,s}^{-1}$
480	Fig 15B.7(b)	Label the horizontal line as T_{g0}, and move the label $T(t)$ to the left of the vertical dotted line $t = t_1$	
483	15C.1, last line	heat-exchange surface	heat-transfer area

485	line 2a	$g_{s,\mathrm{tot}}$	$g_{S,\mathrm{tot}}$
496	Eq 16.3-13	10,400 R	10,400 $^{\mathrm{o}}$R
508	16A.2, line 5	heat energy	energy
509	16A.4(a)	constants.	constants (see §16.6).
509	16B.5, line 4	body at	body initially at
509	16B.5, line 7	*T* of the black body as a function of time	*T*(*t*) of the black body
509	16B.6(c), line 2	values of T_0 and	value of T_0 for
509	16C.1, line 1	**Integration**	**Evaluation**
509	16C.1, line 1	**integral**	**integrals**
524	Eq 17.2-10	g-mol	g-mole
525	Fig 17.3-1	The lower-left sphere should not be shaded and its circumference should be dotted. It should be drawn the same as in Fig. 1.4-1 on p. 24.	
529	2 lines above 17.4-3	$\boldsymbol{\beta}_{AB}$ (b.f. beta)	β_{AB} (l.f. beta, as in line 3a)
529	2 lines above 17.4-4	$\boldsymbol{\beta}_{AB}$ (b.f. beta)	β_{AB} (l.f. beta, as in line 3a)
534	table, LHS of (P)	∇x_a	∇x_α
534	table, LHS of (Q)	$\nabla \omega_a$	$\nabla \omega_\alpha$
537	Table 17.8-1, (U)	$\mathbf{n}_a$	$\mathbf{n}_\alpha$
539	17A.2(c)	17.3-12 and 15	17.3-12, 14, and 15
539	17A.3, line 2	with viscosity	with its viscosity
540	17A.6(a)	chlorine-air	chlorine (*A*)-air (*B*)
540	Prob 17A.8, lines 2 and 5	g-mol	g-mole

540	line after 17A.9-1	as about	to be about
540	17A.9(b)	for Lennard-Jones	for the Lennard-Jones
541	17B.4 (b)	folowing	following
541	17C.1 after 17C.1-2	mass flux with	mass flux of species α with
542	1 line after 17C.2-1	mass flux with	mass flux of species α with
546	Fig., right drawing	Insert a zero ("0") directly below 1.0 on the x_B axis, near z_2	
553	Eq 18.3-14	Move $(k_1'' \text{large})$ one-half inch to the right	
562	6a	$0 < z < L$	$0 \le z \le L$
568	18A.1, line 8	Density of	Density of liquid
569	line 1b	for the measure of	for the measurement of
570	18.A-17, ans	g-mol (twice)	g-mole (twice)
571	18B.4(b)	be of the sum	be the sum
572	Fig caption	The stirrers … maintain	The stirrers maintain
573	18B.8-8, lines 7 & 8	tube, in terms the	tube in terms of the
573	18B.8-8, line 8	of the helium in	of helium in
574	18B.8-10, line 6	60 F	60 ^{o}F
574	18B.8-10, 2 lines below table	lines 2 and 3	rows II and III
574	18B.8-10, 2 lines below table	calculate *A*	calculate *LA*
575	Fig 18B.11, caption	*P* neglected.	*P* may be neglected
576	Eq 18B.13-1	c_{O}	c_0
576	2b	Most such reactions are,	Most of these are, however,

		however, much	
576	fn 11, line 1	Diffusion, *Academic Press*	*Diffusion,* Academic Press
577	18B.14, last line	§18.6	§18.7
577	18B.15, line 2	perimeter *P*, is in	perimeter *P* is in
577	Fig 18B.15(b)	The label on the left arrow should be: $n_{Az}\big\|_z = -\rho \mathscr{D}_{AB} \frac{d\omega_\alpha}{dz}\Big\|_z$	
577	Fig 18B.15(b)	The label on the right arrow should be: $n_{Az}\big\|_{z+\Delta z} = -\rho \mathscr{D}_{AB} \frac{d\omega_\alpha}{dz}\Big\|_{z+\Delta z}$	
578	18B.18, last line	$x_{A1} = 1$ $x_{A2} = 1$	$x_{A1} = 0$ $x_{A2} = 0$
580	Eq 18C.1-4	at $s = \infty$, $c_A = 0$	as $s \to \infty$, $c_A \to 0$
580	Eq 18C.2-1	$0 < r < \kappa R$	$0 \le r < \kappa R$
580	Eq 18C.2-2	$\kappa R < r < R$	$\kappa R \le r \le R$
580	2b, 1b	integrals The integrals may	integrals, which may
581	fn 13, add on	See also T. K. Sherwood and R. L. Pigford, *Absorption and Extraction*, 2nd edition, McGraw-Hill, New York (1952), p. 42.	
589	2 lines above Eq 19.2-3	term)	term, where we set $\rho = \bar{\rho}$)
589	Eq 19.2-3, left side	ρ	$\bar{\rho}$
594	2 lines before 19.4-10	quantities are	indicates quantities
599	1 line after 19.5-3	$\alpha = k/\rho\tilde{C}_p$	$\alpha = k/\rho\hat{C}_p$
601	Eq 19.5-17	at	as

601	Eq 19.5-17	$=$	$\to$	(2 times)
603	Fig caption line 7	(ω_{W1}, T_1)	(T_1, ω_{W1})	
604	Fig caption line 6	all time	all times	
604	19.5-22 to 24	$<$	$\leq$	(8 times)
606	line 4a	at the end of Example 19.4-1	below Eq. 19.4-9	
607	19B.4(b)	$0 < z < \delta(t)$	$0 \leq z \leq \delta(t)$	
608	19D.1, replace	Use… Eq. 19.1-6.	Use the Gauss divergence theorem to obtain Eq. 19.1-6.	
608	19D.1(b)	with local	with the local	
608	Add to fn 2	See also O. T. Hanna, *AIChE Journal*, **8**, 278-279 (1962).		
610	19D.3(a)	Shows that	Show that	
611	line 2a	as $=$	at $\to$	 (2 times)
611	line 3b	higher terms	higher-order terms	
616	horizontal axis in Fig. 20.1-1	D_{AB}	$\mathscr{D}_{AB}$	
618	Fig, ordinate	gm-mol	g-mole	
618	Fig, curve labels	sec	s	(3 times)
620	line before 20.1-59	k'''	k_1'''	
621	Fig, left dwg	Extend arrow down to the liquid-solid interface. Label the interface as $z = 0$.		
621	Fig, left dwg	Remove the curved arrow from "$c_A = 0$ at $t = 0$"		
625	Fig, left end of plate	Install arrows x and y to indicate the coordinate system, exactly as was done on p. 389		
626	Eq 20.2-15	$\Delta < 1$	$\Delta \leq 1$	

627	Fig 20.2-2	Transition region	Transition region*
628	Eq 20.2-24	or y	or as y
628	Eq 20.2-24	=	$\rightarrow$ (four times)
628	Eq 20.2-31	=	$\rightarrow$ (two times)
628	Eq 20.2-31	or y	or as y
628	Eq 20.2-35	at	as
628	Eq 20.2-35	=	$\rightarrow$ (two times)
629	Eq 20.2-40	at	as
629	Eq 20.2-40	=	$\rightarrow$ (two times)
636	Line 2 of Solution	x and z as follows in	x and z in
643	Figure	Remove the arrow below "Parabolic velocity profile in a circular tube"	
643	fn 2	P. C. Chatwin…(1985);	H. B. Fisher, *Ann. Rev. Fluid Mech.,* **5**, 59-78 (1973)
646	Fig, ordinate label	Pé D	Pé_{AB} R
646	Fig, lower RH corner	Taylor solution	Taylor's solution
646	2 lines below Fig	Pé	Pé_{AB}
649	20A.4, 3rd par	liquid water to	liquid water at
650	20B.4, line 3	The solution may be	The solution for the concentration $\rho_A(r,t)$ (r = radial position in spherical coordinates, t = time) may be
652	Before 20B.9-1	at z =	as $z \rightarrow$
652	20B.9-1	=	$\rightarrow$ (2 times)

653	20C.2-2	$r(t)$	$r_s(t)$	
654	Prob 20C.5, line 5	equations to	equations of change to	
654	line after Eq 20D.1-1	funcions	fractions	
655	Eq 20D.2-7 & 8	at $=$	as $\rightarrow$	(2 times) (4 times)
655	20D.3 line 6	creation	production	
655	5 lines before 20D.3-2	pipe	pipe diameter	
656	Eq 20D.4-2	$\left[L-\langle v_z\rangle(t-t')\right]^2)$	$\left[L-\langle v_z\rangle(t-t')\right]^2$	
656	20D.4-3	$0<t<t_0$	$0\leq t\leq t_0$	
661	1 line after 21.4-12	Damkohler	Damköhler	
662	2 lines before 21.4-1	Damkohler	Damköhler	
662	21.4-1 caption	Damkohler	Damköhler	
663	line 1a	Damkohler	Damköhler	
663	line 11a	Damkohler	Damköhler	
669	Eq 21B.2-2	$\dfrac{v_z}{\langle v_z\rangle}$	$\dfrac{\overline{v}_z}{\langle \overline{v}_z\rangle}$	
669	Eq 21B.2-3	$(v_z/\langle v_z\rangle)$	$(\overline{v}_z/\langle \overline{v}_z\rangle)$	
669	Prob 21B.3	$v_z/\langle v_z\rangle$	$\overline{v}_z/\langle \overline{v}_z\rangle$	
669	Prob 21B.3	$\omega_A=\omega_{A0}$	$\overline{\omega}_A=\omega_{A0}$	
669	Prob 21B.3	$\omega_A=\omega_{Ab}$	$\overline{\omega}_A=\overline{\omega}_{Ab}$	
673	Fig 22.1-4	The r coordinate should be indicated by an arrow whose arrowhead ends within the light shaded region.		
678	7 lines after 22.2-8	0.6415	0.6515	

683	line 4a	g-moles	g-mole
683	Eq 22.3-30	g-mol	g-mole
691	above 22.4-20	$0 < r < R$	$0 \le r \le R$
692	1 line after 22.4-35	transferred…interface,	remaining in the sphere at time t,
695	Eq 22.5-7	$\frac{Vk_c}{A\mathscr{D}_{AB}}$	$\frac{Vk_c}{A\mathscr{D}_{AB}} = \mathrm{Sh}$
696	Fig, ordinate	$\frac{Vk_c}{A\mathscr{D}_{AB}}$	delete
715	3 lines after 22.8-52	upstream surface	upstream membrane surface
716	Arrow in figure for “a priori prediction” should point to the lower solid curve		
718	4 lines above 22.9-6	values, so will…however	values, so that the subscript “ref” will not be needed; however
719	5 lines before Eq 22.9-17	Eq. 21.1-10	Eq. 22.1-10
720	1 line after 22.9-23	$\left[\breve{k}_\omega\right]$	$\left[\breve{\mathbf{k}}_\omega\right]$
		The symbol above the letter should be a “klitschka”	
722	22B.1, line 2	at pressure	at a pressure
723	below 22B.3-2	Eqs.,	Eqs.
723	Fig 22B.7	log	$\log_{10}$
723	Fig 22B.7, axis label	C	$^{\circ}$C
723	Fig caption, line 2	DELETE: “under its own vapor”	
724	Below partial ans.	The term in	The term containing
724	Line 10b	$\rho(s)$	$\rho^{(S)}$ (Superscript cap-ess)

724	Line 6b	with	, with
724	line 6b	0.224 ρ_P	0.224 ρ_P,
732	line 2a	only	but
732	1 line after 23.1-31	with respect to z	with respect to x
732	Eq 23.1-35	$\frac{d^2 v}{dz^2} = \frac{1}{z^2(1-z^2)}$	$\frac{d^2 v}{dx^2} = \frac{1}{x^2(1-x^2)}$
733	Eq 23.1-36	$v = (2z-1)\ln\left(\frac{z}{1-z}\right) - 2 + C_1 z + C_2$	$v = (2x-1)\ln\left(\frac{x}{1-x}\right) - 2 + C_1 x + C_2$
733	Eq 23.1-37	$v = (2z-1)\ln\left(\frac{z}{1-z}\right)$	$v = (2x-1)\ln\left(\frac{x}{1-x}\right)$
733	1 line after 23.1-37	$v(1-z) = v(z)$	$v(1-x) = v(x)$
733	1 line after 23.1-37	$v'(1-z) = -v'(z)$	$v'(1-x) = -v'(x)$
733	2 lines after 23.1-35	$v(z)$	$v(x)$
733	4 lines after 23.1-35	$v(z)$	$v(x)$
747	Fig 23.5-6 Fig 23.5.6 caption	$0.1 < x < 0.9$ $0.1 < x < 0.9$	$0.1 \le x \le 0.9$ $0.1 \le x \le 0.9$
748	Fig 23.5-7 Fig 23.5-7 caption	$0.1 < x < 0.9$ $0.1 < x < 0.9$	$0.1 \le x \le 0.9$ $0.1 \le x \le 0.9$
749	Fig 23.5-8 Fig 23.5-8 caption	$0.1 < x < 0.9$ $0.1 < x < 0.9$	$0.1 \le x \le 0.9$ $0.1 \le x \le 0.9$
754	2 line above 23.6-10	Eq. 22.1-3	Eq. 23.1-3
754	line 4b	c_{AS}	c_{As}
758	1 line above 23.6-43	finally[3]	finally
759	23A.1, line 4	F.	^{o}F).

759	Prob 23A.2 line 5	lb-mol	lb-moles
759	Prob 23A.2(d) line 1 Prob 23A.2(d) line 2	moles moles	lb-moles lb-moles
760	line 7a	gm-mol	g-mole
760	Prob 23B.4, line 5	sec^{-1}	s^{-1}
760	Prob 23B.5, line 2	Btu/lb	Btu/lb_m
760	above 22B.5-3	Btu/lb	Btu/lb_m
760	below 22B.5-3	Btu/lb	Btu/lb_m
760	Prob 23B.5, ans	36.5 lbs	36.5 lb_m
760	Lines 1b & 2b	Use 10 … 0.1.	The bottoms composition corresponds to a mole fraction $x_0 = x_W = 0.1$. (???)
761	23C.1(a)	balance for the tank	balance on solute *A* over the tank
768	1 line above 24.2-6	w get	we get
768	6 lines after 24.2-6	can usually be	is often
770	Eq 24.2-10	$x_A \nabla \ln x_A$	$x_A (\nabla \ln x_A)_{T,p}$
774	Eq 24.3-1	$x_A \nabla \ln x_A$	$x_A (\nabla \ln x_A)_{T,p}$
775	1 and 2 lines above 24.4-1	given (Eqs. 24.2-8 or 9):	given by Eqs. 24.2-8 or 9:
777	24.4-6	$\left(1 + \frac{\partial \ln \gamma_P}{\partial \ln x_P}\right)$	$\left(1 + \frac{\partial \ln \gamma_P}{\partial \ln x_P}\right)_{T,p}$
777	24.4-7, line 1	$\left(1 + \frac{\partial \ln \gamma_P}{\partial \ln x_P}\right)$	$\left(1 + \frac{\partial \ln \gamma_P}{\partial \ln x_P}\right)_{T,p}$

777	1 line above 24.4-11	Eqs. 24.4-7, 8, 10, and 11	Eqs. 24.4-7, 8, 10a, and 10b
778	24.4-14	$-c_P v_{\text{migr}}$	$-v_{\text{migr}}\dfrac{\partial c_P}{\partial r}$
778	1 line above 24.4-18	Eqs. 24.4-6, 9, and 10	Eqs. 24.4-6, 10a, and 10b
778	24.4-18	$\left(1+\dfrac{\partial \ln\gamma_{\text{P}}}{\partial \ln x_{\text{P}}}\right)$	$\left(1+\dfrac{\partial \ln\gamma_{\text{P}}}{\partial \ln x_{\text{P}}}\right)_{T,p}$
780	Eq. 24.4-25	$N_{M^+} = N_{X^-} = N_S$	$\mathbf{N}_{M^+} = \mathbf{N}_{X^-} = \mathbf{N}_S$
780	After 24.4-5	…that of the salt *S*, which is conventionally defined in terms of the molar concentrations of salt and water as $c_S/(c_S + c_W)$.	
781	line 1a	Eqs. 24.4-5 and 24	Eqs. 24.4- 24 and 25
781	24.4-26	$x_{M^+}\nabla \ln a_{M^+}$	$x_{M^+}\left(\nabla \ln a_{M^+}\right)_{T,p}$
781	24.4-27	$x_{X^-}\nabla \ln a_{X^-}$	$x_{X^-}\left(\nabla \ln a_{X^-}\right)_{T,p}$
781	24.4-28	$\left(\dfrac{\partial \ln a_{M^+}}{\partial \ln x_S}\right)$	$\left(\dfrac{\partial \ln a_{M^+}}{\partial \ln x_S}\right)_{T,p}$
781	24.4-29	$\left(\dfrac{\partial \ln a_{X^-}}{\partial \ln x_S}\right)$	$\left(\dfrac{\partial \ln a_{X^-}}{\partial \ln x_S}\right)_{T,p}$
781	24.4-30	$\left(\dfrac{\partial \ln\left(a_{M^+} a_{X^-}\right)}{\partial \ln x_S}\right)$	$\left(\dfrac{\partial \ln\left(a_{M^+} a_{X^-}\right)}{\partial \ln x_S}\right)_{T,p}$
781	24.4-33	$\gamma_S = \sqrt{\gamma_{M^+}\gamma_{X^-}}$	$\gamma_S = \gamma_{\pm}$
782	line 1a	Delete line (it duplicates line at bottom of previous page)	
783	24.4-45	$-\dfrac{q_e}{\lambda}$	$\dfrac{q_e \lambda}{\varepsilon}$
783	24.4-46	$-\dfrac{dp}{dr} + \rho_e E_z$	$-\dfrac{dp}{dz} + \rho_e E_z$

783	24.4-47	$\frac{\partial\phi}{\partial z}$	$-\frac{\partial\phi}{\partial z}$
783	line above 24.4-48	Eq. 24.4-36	Eq. 24.4-38
783	Eq 24.4-48	$+\varepsilon$	$-\varepsilon$
783	24.4-49	$\left(\frac{q_e\lambda}{\varepsilon}\right)$	$-\left(\frac{q_e\lambda}{\varepsilon}\right)$
785	fn 9, line 2	241-258	**21**, 241-258
786	line 1a	matrix *m*	membrane *M*
786	before 24.5-2	matrix	membrane (i.e., the "matrix" *m* of Eq. 24.4-5)
786	Eq 24.5-2	v_m	$\mathbf{v}_M$
786	1 line after 24.5-2	v_m	$\mathbf{v}_M$
786	1 line after 24.5-2	matrix	membrane
786	1 line after 24.5-3	matrix *m*	membrane *M*
786	3 lines before 24.5-4	matrix must be considered to be one	membrane must be considered as one
786	24.5-4	$x_\alpha \nabla_{T,p} \ln a_\alpha$	$x_\alpha \left(\nabla \ln a_\alpha\right)_{T,p}$
786	4 lines above 24.5-5	of the matrix	of the membrane
786	24.5-6	$a_{\alpha m}$ p_m ϕ_m	$a_{\alpha M}$ p_M ϕ_M
787	line 1a	*m*	*M*
787	24.5-7	p_m	p_M (2 times)
787	line 4b (main text) line 3b (main text)	matrix matrix-free	"matrix" "matrix-free"
788	3 line above 24.5-8	first law for this system.	first law for this system. For

			simplicity, we omit the directional index, *z*, on the velocities and fluxes.
788	6 lines after 24.5-9	with the matrix	with the membrane
788	7 lines after 24.5-9	occurring	that would occur
788	8 lines after 24.5-9	membrane matrix	membrane
788	Fig 24.5-1	Add labels $z = 0$ and $z = \delta$ to the left and right edges of the "membrane" in the figure, respectively	
789	Eq 24.5-12	$c_{Ae} = K_D c_{Am}$	$c_{AM} = K_D c_{Ae}$
789	2 lines after 24.5-15	of the membrane.	of the membrane (see Fig. 24.5-1).
790	24.5-16\`	$x_S\left(\nabla_{T,p} RT \ln a_S\right)$	$x_S\left(\nabla RT \ln a_S\right)_{T,p}$
790	24.5-17	$x_W\left(\nabla_{T,p} RT \ln a_W\right)$	$x_W\left(\nabla RT \ln a_W\right)_{T,p}$
790	24.5-20	∇p_m	∇p_M
790	1 line after 24.5-20	subscript *m*	subscript *M*
790	24.5-22	$p_e - p_m = \dfrac{RT}{\overline{V}_S} \ln \dfrac{a_{Sm}}{a_{Se}} = \pi_e - \pi_m$	$p_e - p_M = \dfrac{RT}{\overline{V}_S} \ln \dfrac{a_{SM}}{a_{Se}} = \pi_e - \pi_M$
791	line after 24.5-23	where…	(omitting the directional subscript, *z*) where…
791	24.5-24	$\Delta\pi_{\text{eff}} = \left(\pi_{e0} - \pi_{e\delta}\right) - \left(\pi_{m0} - \pi_{m\delta}\right)$	$\Delta\pi_{\text{eff}} = \left(\pi_{e0} - \pi_{e\delta}\right) - \left(\pi_{M0} - \pi_{M\delta}\right)$
791	24.5-25	$\left(1 + \dfrac{\partial \ln \gamma_s}{\partial \ln x_s}\right) \dfrac{dx_s}{dz}$	$\left(1 + \dfrac{\partial \ln \gamma_S}{\partial \ln x_S}\right)_{T,p} \dfrac{dx_S}{dz}$
792	24.5-27	$\ln \dfrac{a_{We}}{a_{Wm}} = \dfrac{\overline{V}_W}{RT}\left(p_m - p_e\right) = \dfrac{\overline{V}_W}{RT} \Delta\pi$	

			$\ln\frac{a_{We}}{a_{WM}}=\frac{\overline{V}_W}{RT}\left(p_M-p_e\right)=\frac{\overline{V}_W}{RT}\left(\pi_M-\pi_e\right)=\frac{\overline{V}_W}{RT}\Delta\pi$
792	line after 24.5-27	subscripts e and m	subscripts e and M
792	24.5-28	$\frac{a_{Se}}{a_{Sm}}=\frac{x_{M^+e}x_{X^-e}}{x_{M^+m}x_{X^-m}}\frac{\gamma_{Se}}{\gamma_{Sm}}=\exp\left(\frac{\overline{V}_S}{RT}\Delta\pi\right)$	$\frac{a_{Se}}{a_{SM}}=\frac{x_{M^+e}x_{X^-e}}{x_{M^+M}x_{X^-M}}\left(\frac{\gamma_{Se}}{\gamma_{SM}}\right)^2=\exp\left(\frac{\overline{V}_S}{RT}\Delta\pi\right)$
792	24.5-29	$\frac{c_{M^+e}c_{X^-e}}{c_{M^+m}c_{X^-m}}=K_D=\left(\frac{\gamma_{Sm}}{\gamma_{Se}}\frac{c_m}{c_e}\right)^2\exp\left(\frac{\overline{V}_S}{RT}\Delta\pi\right)$	$\frac{c_{M^+e}c_{X^-e}}{c_{M^+M}c_{X^-M}}=K=\frac{\gamma_{SM}}{\gamma_{Se}}\left(\frac{c_e}{c_M}\right)^2\exp\left(\frac{\overline{V}_S}{RT}\Delta\pi\right)$
792	24.5-30	$c_{Sm}^2+c_{Sm}c_{X^-m}=\frac{1}{K_D}c_{Se}^2$	$c_{SM}^2+c_{SM}c_{X^-M}=\frac{1}{K}c_{Se}^2$
792	after 24.5-30	…solution.	…solution (K is of order unity for monovalent ions).
792	24.5-31	$\phi_m-\phi_e=\left(\frac{z_{M^+}F}{RT}\right)\ln\frac{x_{M^+m}}{x_{M^+e}}$	$\phi_M-\phi_e=-\left(\frac{RT}{z_{M^+}F}\right)\ln\frac{x_{M^+M}}{x_{M^+e}}$
795*	above 24.6-10	$\psi=p_N/p_0$	$\psi_N=p_N/p_0$
796*	Fig 24.6-1 ordinate label	Dimensionless pressure ψ	Dimensionless total pressure $\psi=\psi_N+\psi_H$
796*	after 24.6-13	The results are	The results for $\psi_{N2}+\psi_{H2}$ and $\psi_{N1}+\psi_{H1}$
796*	Eq 24.6-13	$\psi_{H2}=\frac{1}{2}\left(1+e^{-7.48\tau}\right)$	$\psi_{H2}=\frac{1}{2}\left(1-e^{-7.48\tau}\right)$
796*	Eq 24.6-13	$\psi_{H1}=\frac{1}{2}\left(1-e^{-7.48\tau}\right)$	$\psi_{H1}=\frac{1}{2}\left(1+e^{-7.48\tau}\right)$

797	Table, cols 2 & 3	Delete superscripts *a* and *b*	
798	24.6-18	$\mathscr{D}_{AB}^{\text{ext}} = Ð_{AB}^{\text{ext}}\left(1+\frac{\partial \ln\gamma_A}{\partial \ln x_A}\right)$	$\mathscr{D}_{AB}^{\text{ext}} = Ð_{AB}^{\text{ext}}\left(1+\frac{\partial \ln\gamma_A}{\partial \ln x_A}\right)_{T,p}$
799	24A.3	$F = 96{,}500$	$F \doteq 96{,}500$
799	Prob 24B.1 line 2	Eq. 25.4-50	Eq. 24.4-50
799	line 1b	estimate junction	estimate the junction
800	Above 24B.3-1	Calculate the distribution coefficient of	Calculation the equilibrium constant for the distribution of temperature,
800	Eq 24B.3-1	K_D	K
800	24B.3 Ans	0.633	0.64
800	24B.4, line3	pure water,	pure water at room temperature,
800	Prob 24B.6 line 3	of the transport to the	of the transport due to the
800	Prob 24B.6 line 4	24.6-3	24.6-1
800	Eq 24B.6-1	∇p	∇p_A
800	Eq 24B.6-2	$\frac{\varepsilon a}{\tau}$	$\frac{1}{1-\varepsilon}\,\frac{\varepsilon a}{\tau}$
801	line 4a	Eq. 24.2-9, and also the auxiliary	Eq. 24.2-9. The auxiliary
801	2 lines above 24C.3-1	dilution) are	dilution) for Na^+ and Cl^- are
802	24C.4-2	$\frac{F}{\varepsilon}$	$-\frac{F}{\varepsilon}$
802	fn 4	(1991), p. 256.	(1991).

803	line 3a	The field	The potential field
803	24C.7, line 1	cellophane	cellophane membrane
803	Prob 24C.7 line 2	assume glucose	assume the glucose
803	24C.7, listing	$\overline{V}_s$	$\overline{V}_g$
803	Prob 24C.8 line 1	of the hypothetical	of a hypothetical
803	24C.8, line 2	1.0	0.1
803	24C.7, answer	0.00242	0.00234
803	24C.8, ans	product solute concentration	solute mole fraction in the filtrate
803	Fig 24C.9	Remove the word "Distance" from the figure, and add $z = 0$ next to the vertical line just to the left of "Membrane" and add $z = \delta$ next to the vertical line just to the right of "Membrane". These additions should be put in the space where the word "Distance" was deleted.	
814	Ex 2(d) Ex 2(e)	$(\boldsymbol{\delta}_1 \cdot \mathbf{v})$ $[\boldsymbol{\delta}_1 \times \mathbf{w}]$	$(\boldsymbol{\delta}_x \cdot \mathbf{v})$ $[\boldsymbol{\delta}_x \times \mathbf{w}]$
819	Ex 1(f)	$[\boldsymbol{\tau} \cdot \boldsymbol{\delta}_1]$	$[\boldsymbol{\tau} \cdot \boldsymbol{\delta}_x]$
822	Eq A.4-32	${}_i\sum\sum_j$	$\sum_i\sum_j$
825	Ex 4, line 1	ε_{ijk} (wrong font)	ε_{ijk} (lightface)
827	Fig A.6-2	δ_r δ_θ	$\boldsymbol{\delta}_r$ $\boldsymbol{\delta}_\theta$
827	3 lines after A.615	i.e., v	i.e., $\mathbf{v}$ (boldface Roman)
828	Ex 1, 1st equation	**0** (boldface)	0 (lightface)

838	Line 1a	∇v	$\nabla \mathbf{v}$
838	Eq A.7-24 (rt side)	$[\cdots]$	$[\cdots]_r$
838	Eq A.7-27 (rt side)	$\dfrac{1}{r\sin\phi}$	$\dfrac{1}{r\sin\theta}$
841	Eq A.8-8	$\sin\theta d\theta$	$d\theta$
845	fn to Table B.2	$\mathbf{q}$	$-k\nabla T$
847	Eq B.5-8	$[...)+\rho g_\theta$	$[...]+\rho g_\theta$
849	Table B.7, title	Φv	Φ_v
851	Table B.11, title	Both ω and ρ should be light face	
851	Table B.11, last line of fn	$x_B R_A - x_A R_\beta$	$x_B R_A - x_A R_B$
856	Fig C.5-1	In both drawings, the *x*-axis and *y*-axis should be labeled.	
856	Fig C.5-1, right dwg	$\coth\theta = 1/\coth\theta$	$\coth\theta = 1/\tanh\theta$
864	Table heading col 9	μ_c $(\mathrm{g/cm \cdot s} \times 10^6)$	$\mu_c \times 10^6$ $(\mathrm{g/cm \cdot s})$
864	Table heading col 10	k_c $(\mathrm{cal/cm \cdot s \cdot K} \ \times 10^6)$	$k_c \times 10^6$ $(\mathrm{cal/cm \cdot s \cdot K})$
865	fn h	^{h}Values	^{h} Values
878	Damköhler	626	626, 661
879	Hanna	431	429
893	Tensor, unit	817	19, 817

Back cover, top diagram: $\$_{AB}$ $\mathscr{D}_{AB}$

	$\dfrac{dy}{d\omega_A}$	$\dfrac{d\omega_A}{dy}$
Back cover, middle diagram:	$\dfrac{dy}{dv_x}$	$\dfrac{dv_x}{dy}$
Back cover, bottom diagram:	$\dfrac{dy}{dT}$	$\dfrac{dT}{dy}$

MISPRINTS:

25	fn 2, line 6	edition 1970),	edition (1970),
32	fn 3, line 1	Vol. 1,	Vol. 1
32	fn 4, line 1	Vol. 1,	Vol. 1
37	fn 1, line 1	*Revs.*	*Revs.*,
38	fn 2, line1	*Chem.*	*Chem.,*
70	fn 6, line 2	(1965)	(1965);
96	fn 6, line 2	Vol. 1.,	Vol. 1,
110	3C.1, line 1	(Fig. 3C.-1)	(Fig. 3C.1)
122	fn 3, line 6	386-391	386-391 (1970)
125	fn 4	*Mech.* (twice)	*Mech*., (twice)
135	fn l, line 8	*Mechanics*,"	*Mechanics*,
140	fn 9, line 3	…*Theory*, Springer…	…*Theory*, 8th edition, Springer…
142	4B.2, line 2	4.1.1	4.1-1
149	fn 6	McGraw-Hill (1937)	McGraw-Hill, New York (1937)
153	fn 2, line 2	McGraw-Hill (1961)	McGraw-Hill, New York (1961)

166	fig capt, last line	(1950)}.	(1950)].
182	fig capt, line 1	6.1-3.	6.1-3).
187	fig capt, line 3	*Handbook*,	*Handbook*
196	3 lines below 6C.3-2	baffles,	baffles
196	fn 8, line 2	Press, (1967),	Press (1967),
232	fn 1, line 2	Vol. 1.,	Vol. 1,
235	fn 5, line 1	*Sci.*	*Sci.,*
235	fn 5, line 3	*Rheol.*	*Rheol.,*
235	fn 6, line 2	*Mech.*	*Mech.,*
235	fn 6, line 3	(1985), 102-105.	(1985), pp. 102-105.
242	fn 4, line 2	*Vol. 1.*	*Vol. 1,*
245	fn 1	*Restitutiva* (1678)	*Restitutiva*, London (1678)
274	fn 1, line 5	edition (2000).	edition, Oxford University Press (2000).
289	fn 7, line 4	corrections (1964).	corrections, Wiley, New York (1964).
311	Fig 10.8-1, left side, #2	2	2.
326	line 1b	r_1 respectively and	r_1, respectively, and
349	fn 4, line 1	Malabar Fla.	Malabar, Fla.
353	fig caption	wave, for helium	wave for helium
353	fig caption	p. 333]	p. 333.]
372	fn 14	*Chem.*	*Chem.,*
385	fn 15, line2	et seq;	et seq.; (style??)
400	fn 4	Co., (1946),	Co. (1946),

404	Table 12D.2, fn a	McGraw-Hill (New York).	3rd edition, McGraw-Hill, New York (1998).
428	fn 1, line 2	New York, (1977),	New York (1977),
428	fn 1, line 3	**74**, (35)	**74** (35),
428	fn 1, line 4	**75,** (1),	**75** (1),
437	Eq 14.3-18	10,000}	10,000)
446	Fig 14.7-1	Remove horizontal line just above T_d	
450	Col 1, line 3	$T(\mathrm{C})$	$T(^\circ\mathrm{C})$
482	fn 2, line 5	Fla., (1983),	Fla. (1983),
488	fn 3, line 4	edition,	edition
493	fn 1, line 1	edition,	edition
495	fig capt, line 6	(1901).	(1901).]
500	Fig 16.4-4, caption	McAdams	McAdams,
505	fn 2, line1	Ed.	ed.
514	fn 1, line 2	*Reson.*	*Reson.,*
519	fn 7, line 1	*Rev.*	*Rev.,*
523	fn 5	B. A. Ivakin, P. E. Suetin	B. A. Ivakin and P. E. Suetin
527	fn 7, line 3	*Phys.*	*Phys.,*
529	fn 9, line 4	*Phys.*	*Phys.,*
540	17A.9(a),, line 3	for $(c\mathscr{D}_{AA^*})_c$	for $(c\mathscr{D}_{AA^*})_c$. (add period after formula)
570	Prob 18A.6(b)	Eq. 17-2-1	Eq. 17.2-1
611	fn 10, line 1	Spalding ed.),	Spalding, ed.),
621	fn 11, line 2	Cliffs N.J.	Cliffs, N.J.

638	Fig caption	AIChE Journal	*AIChE Journal*
647	fn 13	*Chromatog*. **589**	*Chromatog*., **589**
648	fn 1	*Chem.* **42,**	*Chem.*, **42**,
685	fn 3, line 2	New York,	New York
764	fn 1, line 1	*Wien*	*Wien*,
793	fn 1 (a)	Vols. 1 and 2 Oxford	Vols. 1 and 2, Oxford
854	2nd equation	C.2.3	C.2-3